



# **Metropolitan Water Reclamation District of Greater Chicago**

**Welcome to the May  
Edition of the 2021  
M&R Seminar Series**

# NOTES FOR SEMINAR ATTENDEES

- All attendees' audio lines have been muted to minimize background noise.
- A question and answer session will follow the presentation.
- Please use the "Chat" feature to ask a question via text to "All Panelists".
- The presentation slides will be posted on the MWRD website after the seminar.
- The ISPE has approved this seminar for one PDH, and the IEPA has approved this seminar for one TCH. Certificates will only be issued to participants who attend the entire presentation.

# **Belinda Sue McSwain Sturm, Ph.D.**

Associate Vice Chancellor for Research  
Professor of Civil, Environmental & Architectural Engineering  
The University of Kansas  
Lawrence, Kansas



Dr. Belinda Sturm is a Professor in the Department of Civil, Environmental & Architectural Engineering at the University of Kansas. She also serves as an Associate Vice Chancellor for Research. Belinda currently serves as Vice-Chair of the Water Environment Federation's Municipal Design Symposium and as Chair of the International Water Association's USA National Committee Executive Board. Belinda earned her bachelor of science in Public Health from the University of North Carolina at Chapel Hill and her Ph.D. in Civil Engineering and Geological Sciences from the University of Notre Dame.



# **Recent Advances in Aerobic Granular Sludge Processes**

**Belinda Sturm, PhD  
University of Kansas**

# Steady Progression of Design for Settleability

Selector zone concept introduced to control bulking (Choduba et al. 1973)

Filaments shown to dominate based on bioreactor design and operation (Eikelboom, 1975)

Unified theory of filaments developed (Sezgin et al, 1978)

DO shown to impact selection of filaments versus flocs (Palm et al. 1980)

SVI correlations for settling curves became more standardized (Wahlberg and Keinath, 1998; Daigger, 1995; Ozinsky and Ekama, 1995)

Selector zone design became more formal (Marten and Daigger, 1997) and better understood (Martins et al, 2004)

WE&RF report on selector zone design guidelines (Gray et al, 2008)

Is aerobic granular sludge the natural evolution of good settling sludge development?

1970s

1980s

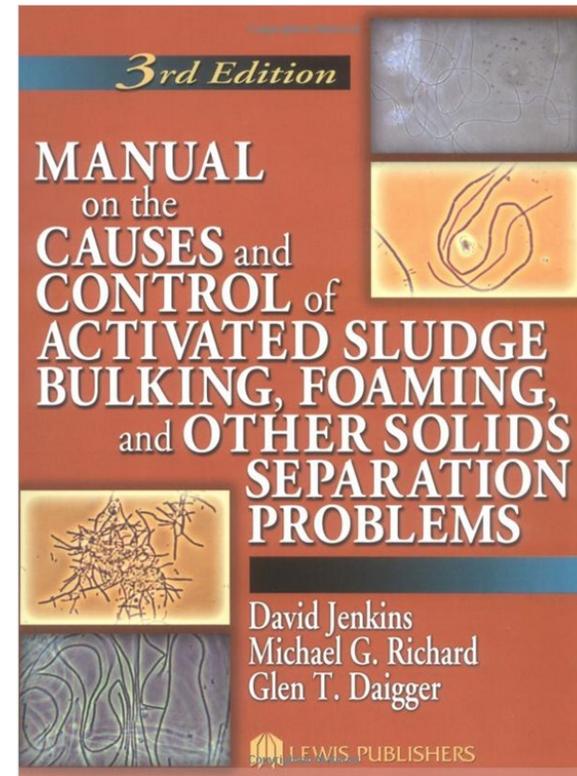
1990s

2000s

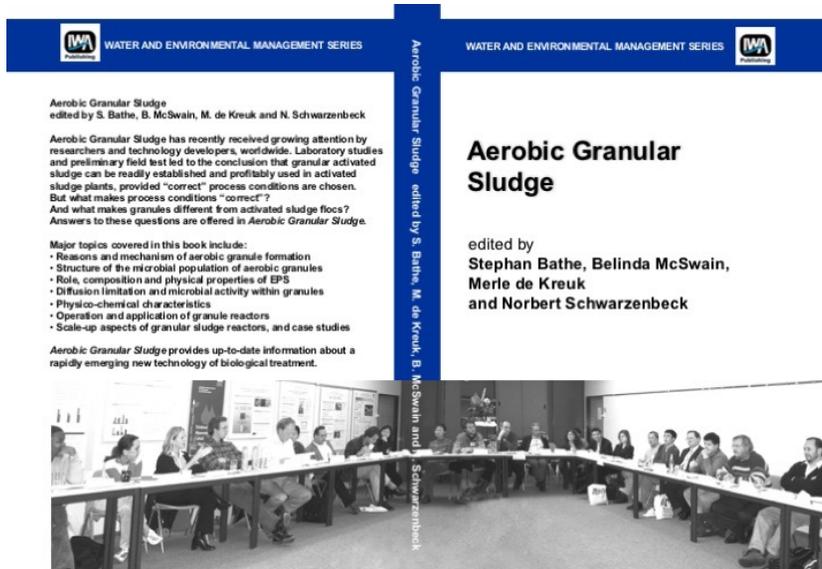
2010s

## Five decades of settling theory evolution has been summarized in one key manual for operations

- Focus: settleability
  - Select for good settling
    - Low SVI
    - Larger floc
    - Limit filamentous growth
- Operating parameters
  - SRT control
  - F/M gradients
  - Selector zones and plug flow



# IWA Granule Workshop 2004

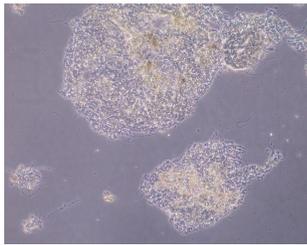


*Granules making up aerobic granular activated sludge are to be understood as aggregates of microbial origin, which do not coagulate under reduced hydrodynamic shear, and which subsequently settle significantly faster than activated sludge flocs.*

- $SVI_{30} < 60 \text{ mL/g}$
- $SVI_5 = SVI_{30}$  or  $SVI_5 / SVI_{30} = 1$
- Settling velocities  $> 9 \text{ m/hr}$
- Particle diameter  $> 200 \mu\text{m}$

# How Does Densified Activated Sludge Compare with Granular Sludge?

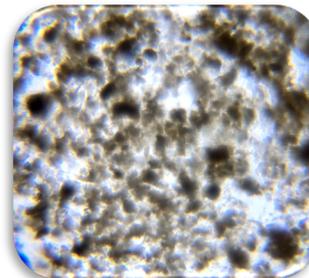
*Compact AS  
(non-granular)*



SVI<sub>30</sub> 80 to 120 mL/g

**non-patented AS**  
Conventional Selector  
Design

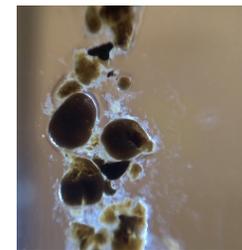
*Densified AS  
(non-granular)*



SVI<sub>30</sub> < 80 mL/g

**non-patented AS\***

*Densified AS  
(granular)*



SVI<sub>30</sub> < 50 mL/g

**AquaNEREDA™**  
**inDENSE™**

# Different types of **aerated** granules have been formed

| Parameter                      | NIT Granules                   | OHO Granules                               | NDN-OHO Granules                      | NDN-PAO Granules*  |
|--------------------------------|--------------------------------|--|---------------------------------------|--|
| <b>Processes</b>               | Nitrification (low COD/N feed) | COD oxidation (and possibly Nitrification) | Nitrification + Denitrification       | Nitrification + Denitrification + EBPR <sup>1</sup>                    |
| <b>Feeding condition</b>       | Aerobic                        | Aerobic                                    | Anoxic                                | Anaerobic  |
| <b>Denitrifying bacteria</b>   | N/A                            | OHOs <sup>2</sup>                          | OHOs <sup>2</sup>                     | PAOs <sup>3</sup> and GAOs <sup>4</sup>                                |
| <b>Nitrogen removal method</b> | N/A                            | Assimilation w/ limited denitrification    | Sequential anoxic and aerobic periods | Simultaneous nitrification and denitrification (SND) in aerobic period |
| <b>Demonstrated</b>            | Lab-scale                      | Lab-scale                                  | Lab-scale                             | Lab- and Full-scale  |

1. EBPR – Enhanced biological phosphorus removal
2. OHOs – Ordinary heterotrophic organisms
3. PAOs – Phosphorus accumulating organisms
4. GAOs – Glycogen accumulating organisms – may also grow

**Figdore, B.A.,** Stensel, H.D., Winkler, M.K.H., Neethling, J.B. (2017) *Aerobic Granular Sludge for Biological Nutrient Removal*. Project No. NUTR5R14h. Water Environment and Reuse Foundation: Alexandria, VA.

# Implementation of Aerobic Granular Sludge in Continuous Flow Activated Sludge (CFAS) Plants

## Aerobic granular sludge SBRs

- Sequencing batch operations
- High anaerobic F/M Ratio
- Short settling time

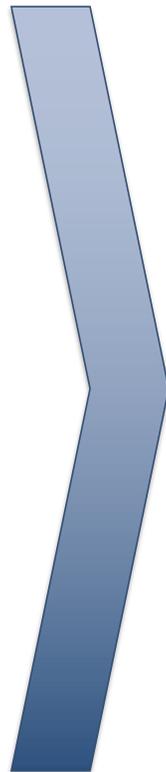
## Conventional activated sludge

- Continuous flow
- Can have high anaerobic F/M with selector
- No settling selection

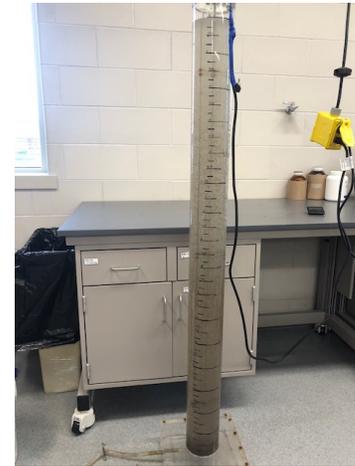


## **Densifying Activated Sludge Is Key to Increasing Capacity at WRRFs**

# Lawrence WWTP Granular Sludge Pilot (70 L)



Flocculent Sludge  
– 5 mins Settling



Granular Sludge  
– 5 mins Settling



Flocculent Sludge  
– 30 mins Settling

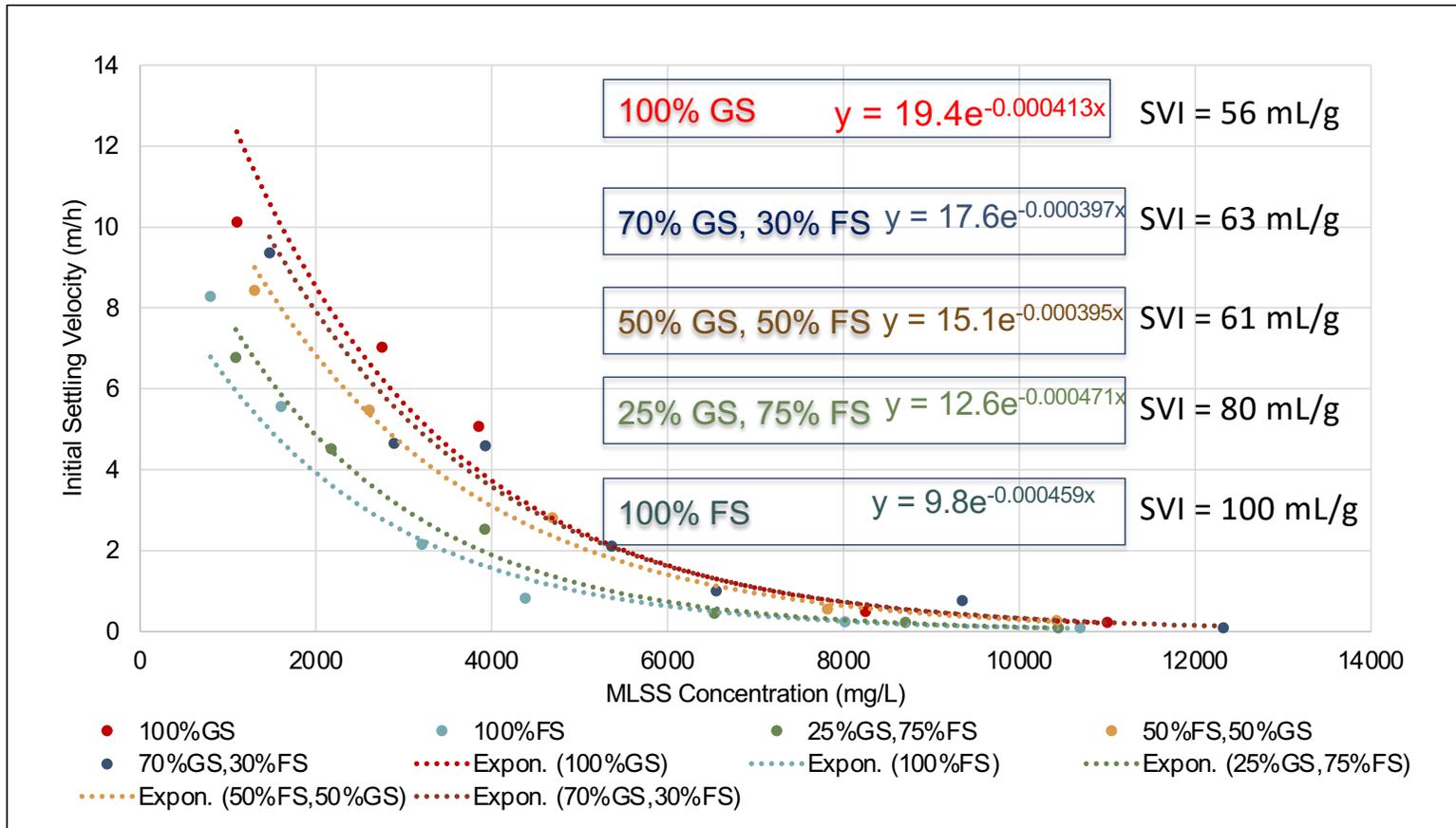


Granular Sludge  
– 30 mins Settling

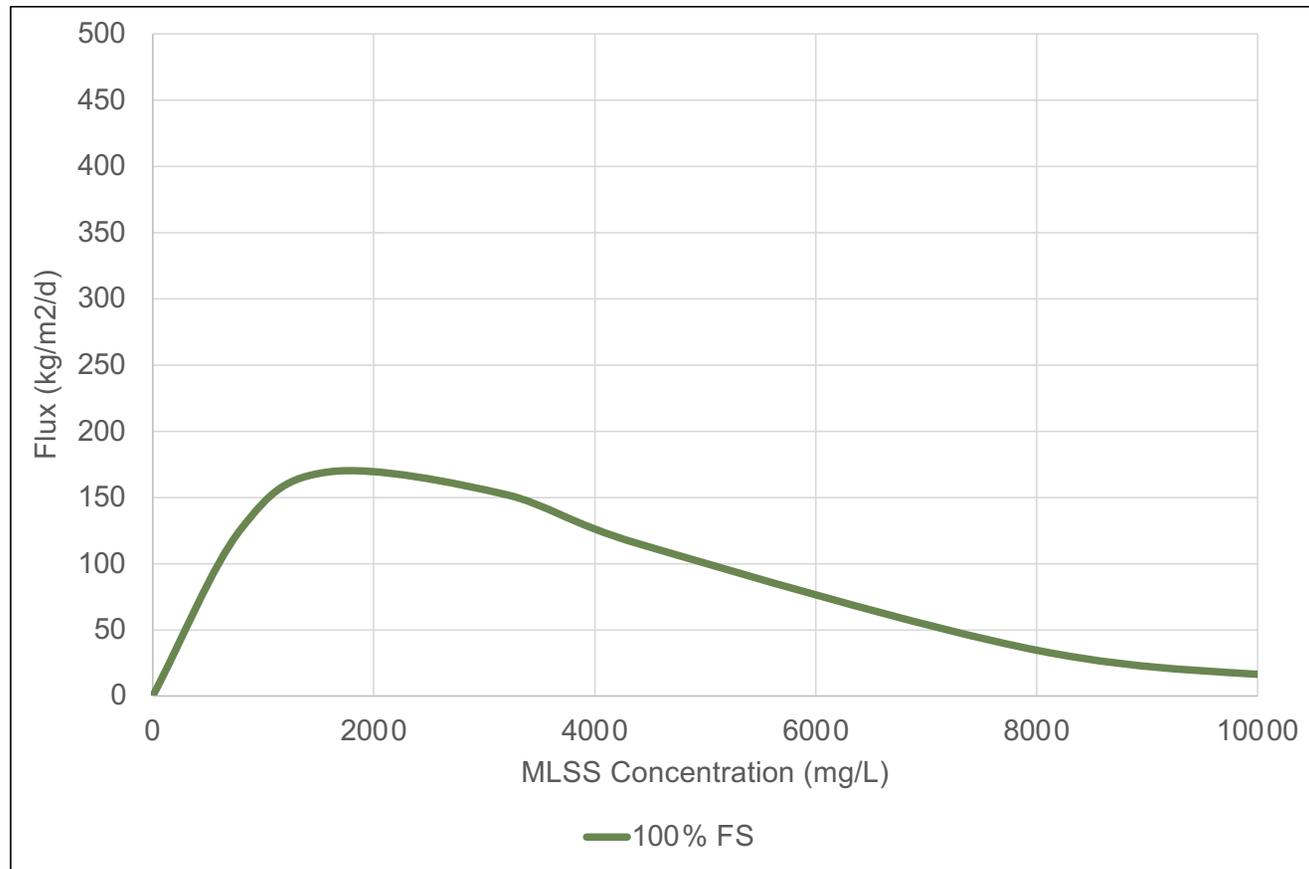
**WERF U1R14 Project**

# Lawrence WWTP AGS Pilot Results - Settling Parameters

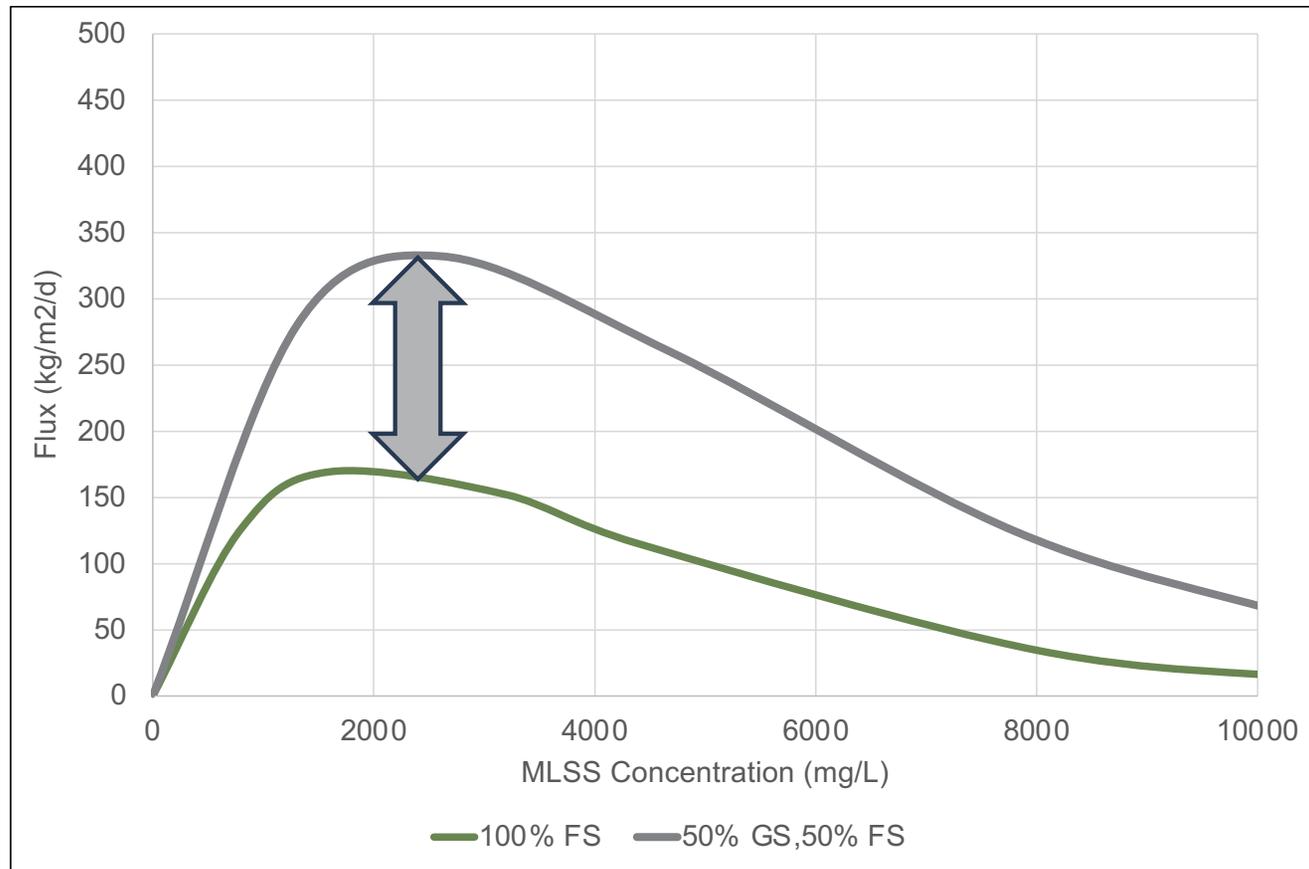
$$V_s = V_0 \cdot e^{(-K \cdot X_{TSS})}$$



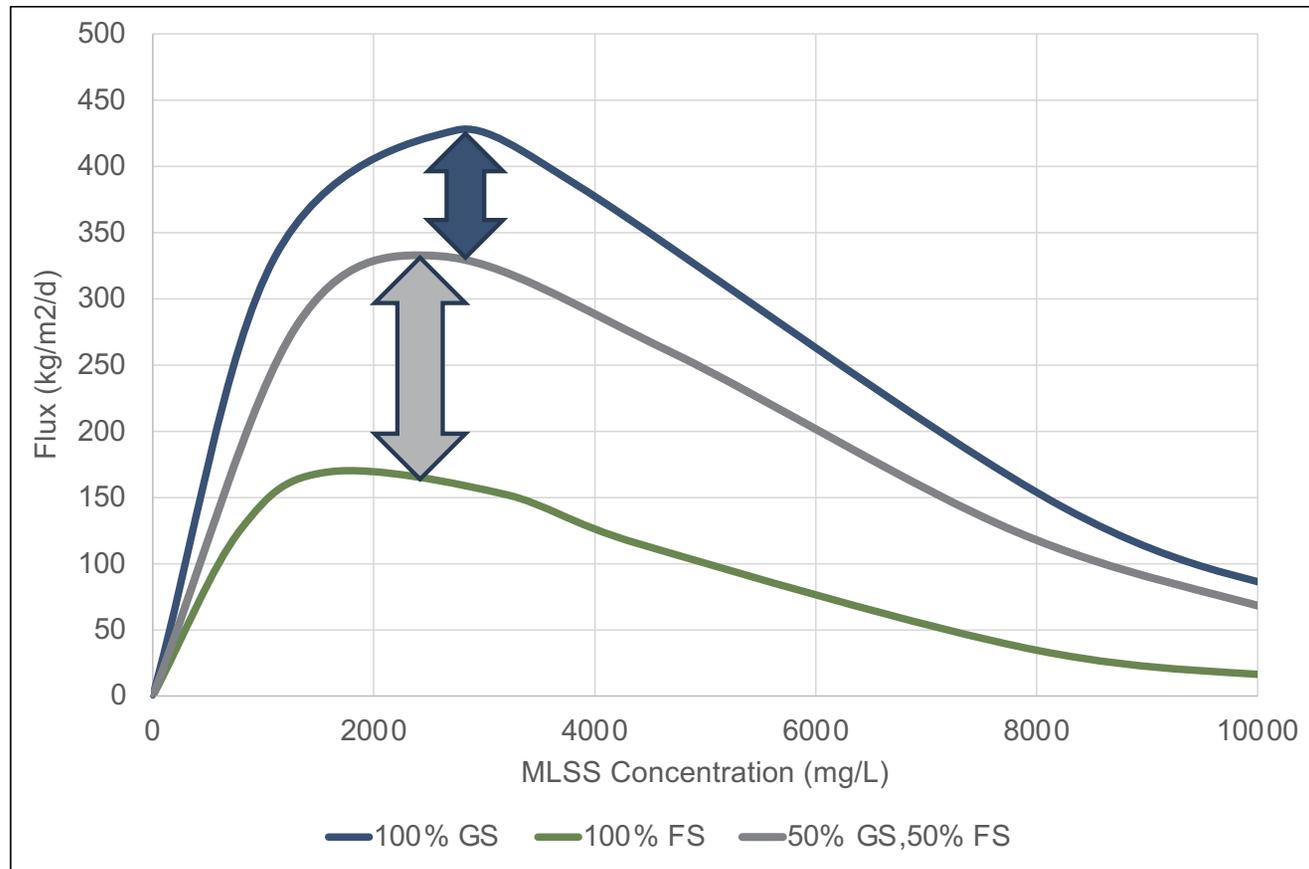
## Flux Curves for different levels of granulation



## Flux Curves for different levels of granulation



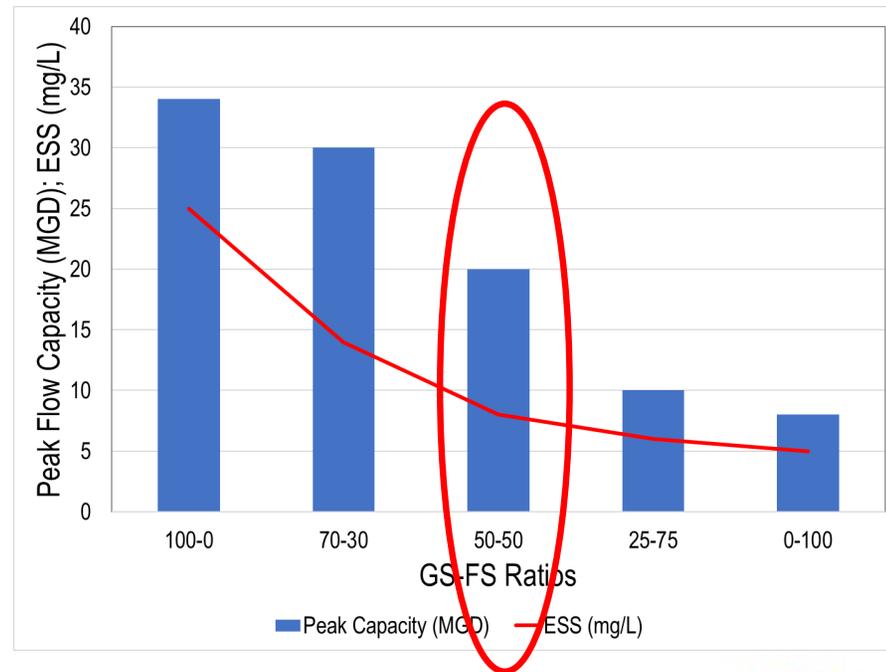
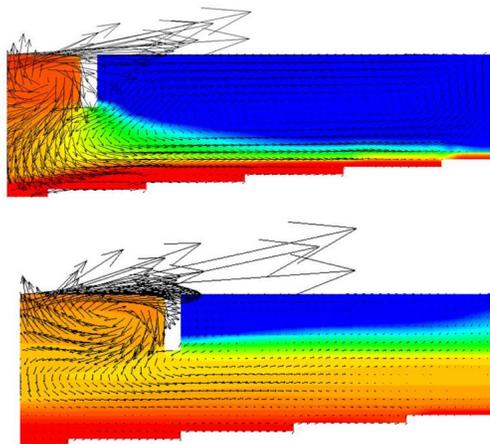
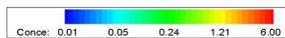
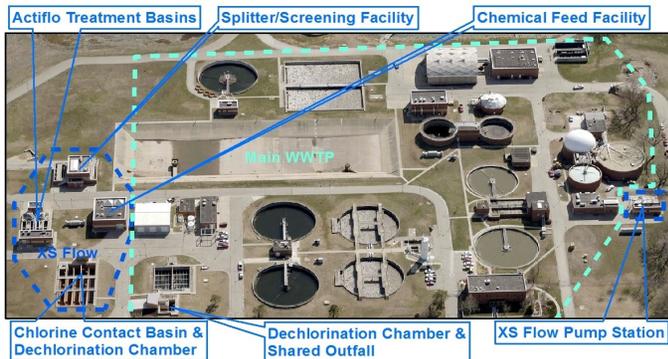
## Flux Curves for different levels of granulation



# Clarifier Capacity Modeling Hazen



Performed by Dr. José Jimenez  
and Dr. Alonso Griborio



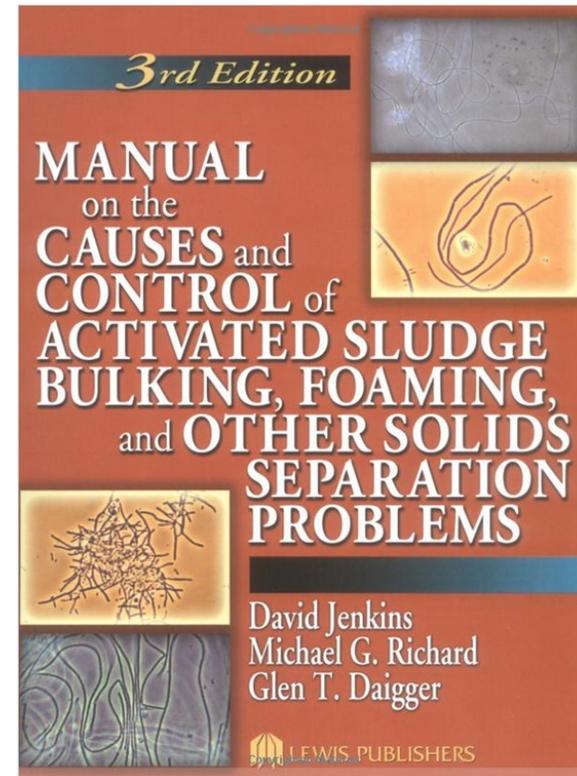
Note: Modeling assumed equal biomass concentrations for all ratios



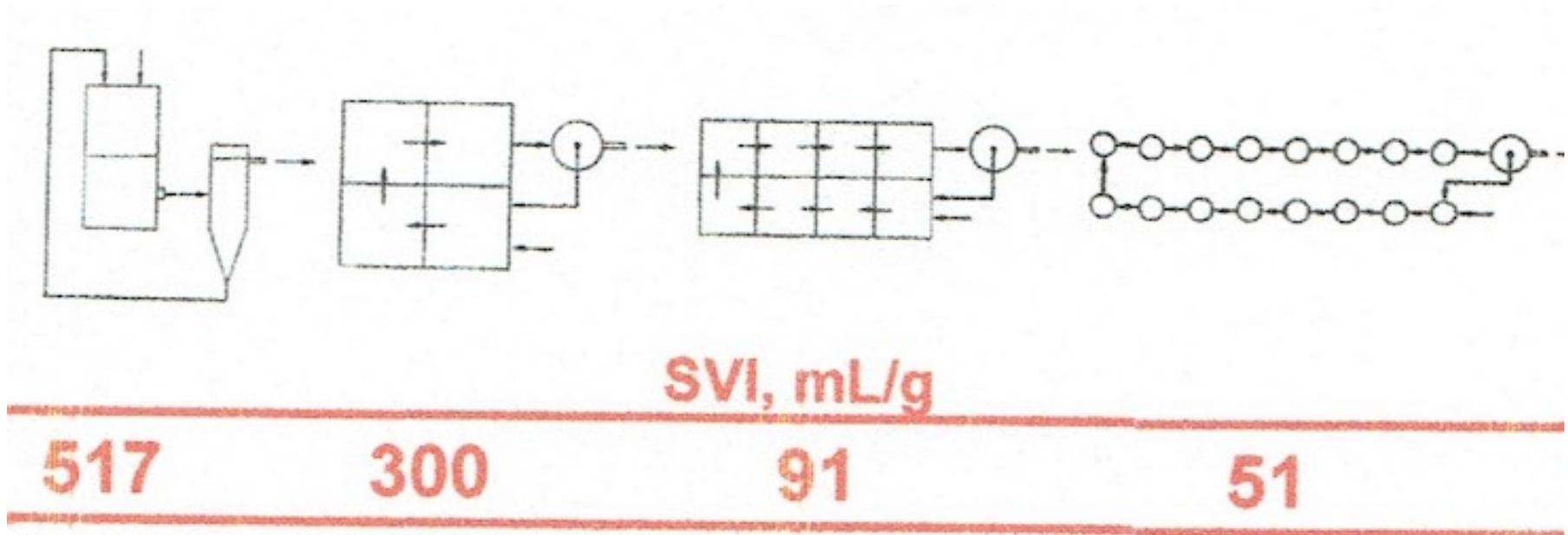
**Sludge Densification extends the same principles we learned from preventing bulking sludge**

## Five decades of settling theory evolution has been summarized in one key manual for operations

- Focus: settleability
  - Select for good settling
    - Low SVI
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- Operating parameters
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  - Selector zones and plug flow

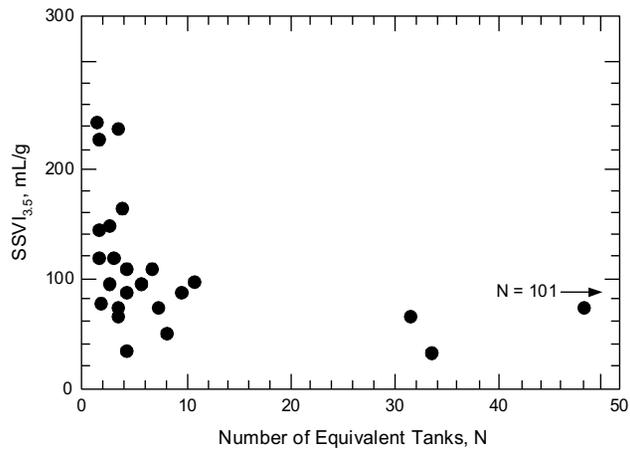


## Floc Selection Theory and Filament Out-Selection



Chudoba, Ottova and Madera (1973) *Water Research*, 7, 1163.

# What are our key parameters for selecting for good settling activated sludge?

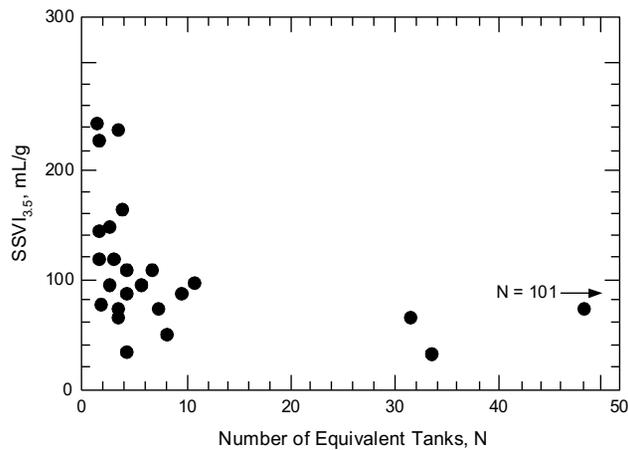


*From E. J. Tomlinson and B. Chambers, The effect of longitudinal mixing on the settleability of activated sludge. Technical Report TR 122, Water Research Centre, Stevenage, England, 1978. Reprinted by permission of the Water Research Centre.)*

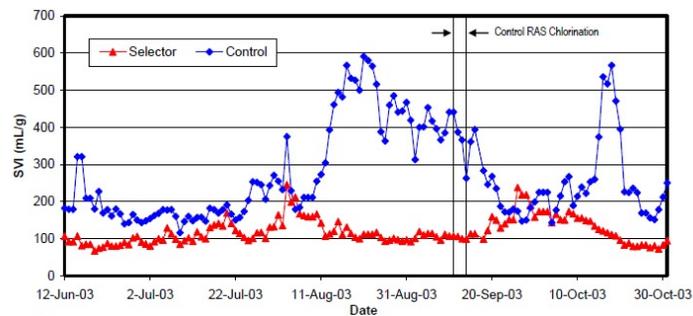
## 1. Plug Flow Conditions

Slide courtesy of Dr. Leon Downing,  
Black & Veatch

# What are our key parameters for selecting for good settling activated sludge?



From E. J. Tomlinson and B. Chambers, *The effect of longitudinal mixing on the settleability of activated sludge*. Technical Report TR 122, Water Research Centre, Stevenage, England, 1978. Reprinted by permission of the Water Research Centre.)



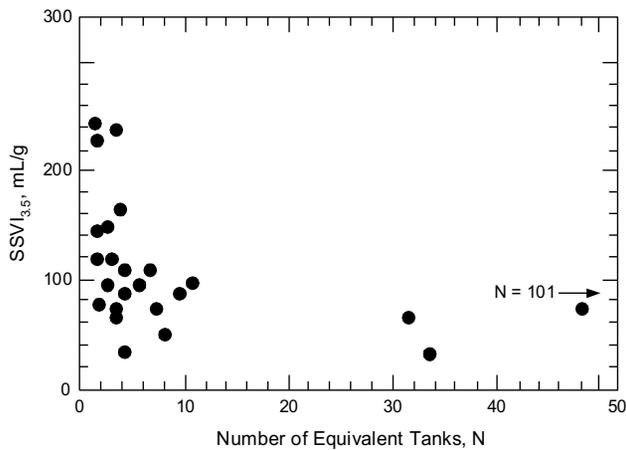
From Gray et al (2006) *Develop and Demonstrate Fundamental Basis for Selectors to Improve Activated Sludge Settleability*

**1. Plug Flow Conditions**

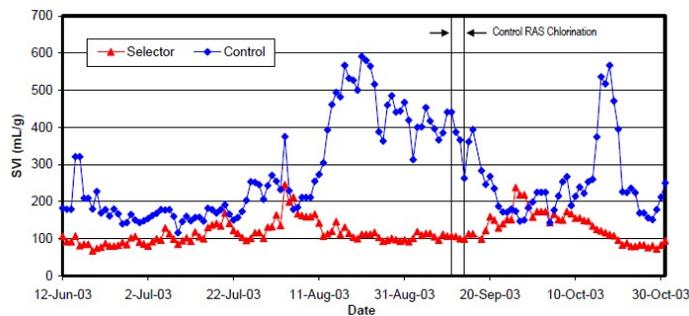
**2. Anaerobic/Anoxic feed**

Slide courtesy of Dr. Leon Downing,  
Black & Veatch

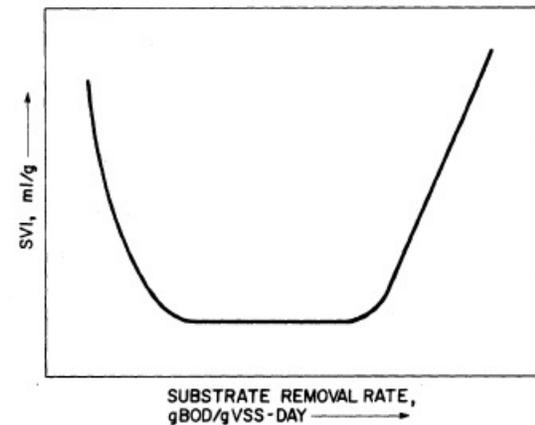
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From E. J. Tomlinson and B. Chambers, *The effect of longitudinal mixing on the settleability of activated sludge*. Technical Report TR 122, Water Research Centre, Stevenage, England, 1978. Reprinted by permission of the Water Research Centre.)



From Gray et al (2006) *Develop and Demonstrate Fundamental Basis for Selectors to Improve Activated Sludge Settleability*



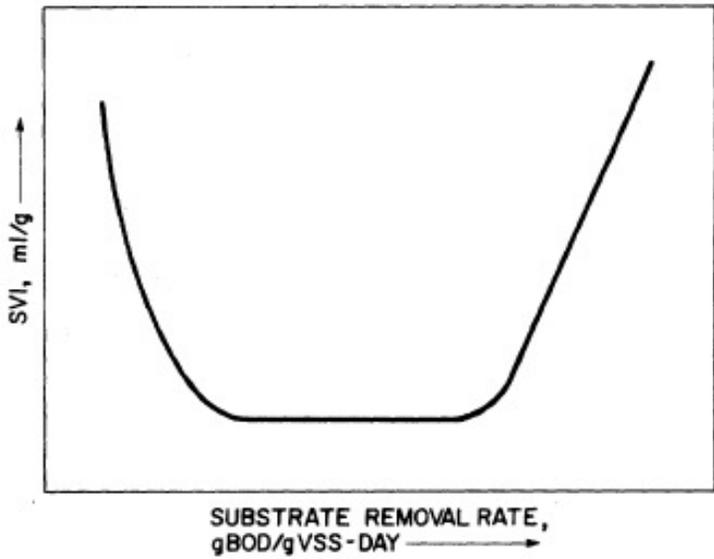
**FIGURE 15. Effect of substrate removal rate on sludge volume index.**

From Sezgin et al (1978) *A Unified theory of activated sludge bulking*. *Journal of Water Pollution Control Federation* 50(2)

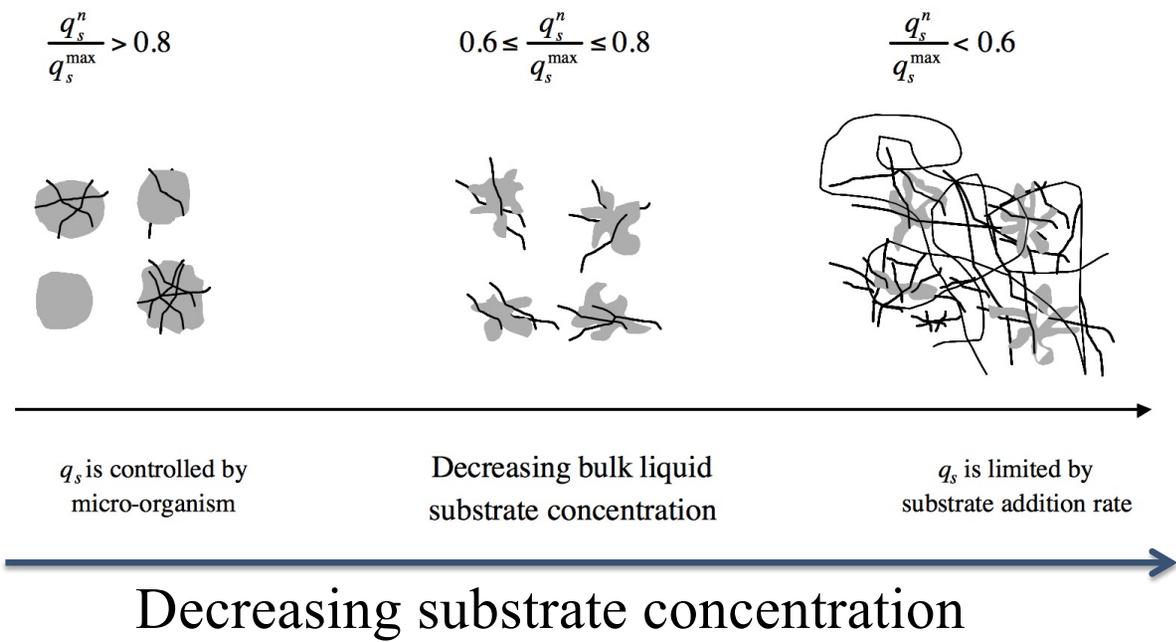
1. Plug Flow Conditions
  2. Anaerobic/Anoxic feed
  3. Loading rate matters
- Slide courtesy of Dr. Leon Downing, Black & Veatch

# High F/M and Metabolic Selection

$$q_s = q_s^{\max} \frac{C_s}{K_s + C_s}$$



**FIGURE 15.** Effect of substrate removal rate on sludge volume index.



From Sezgin et al (1978) A Unified theory of activated sludge bulking, Journal of Water Pollution Control Federation 50(2)

Martins et al. (2003) *Water Research* 37, p.2555–2570

# A high F/M anaerobic feeding regime is important to drive diffusion into granule and achieve metabolic selection

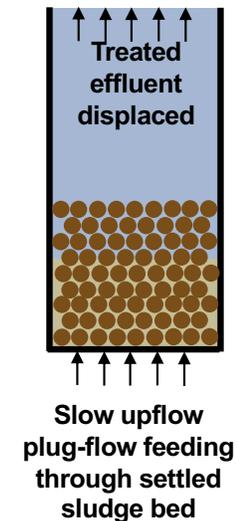
Contacting with high rbCOD drives diffusion to granule interior

-Allows interior to be biologically active

Anaerobic feeding selects for PAOs for EBPR

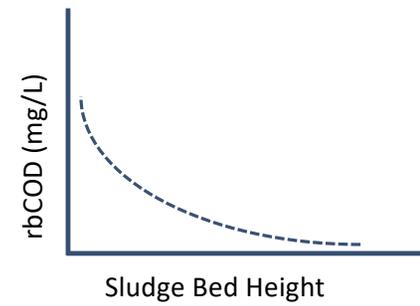
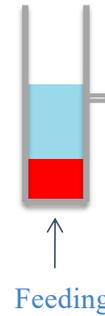
Slow upflow feeding widely used in lab and full-scale SBRs

Slug feeding has also been used in lab systems

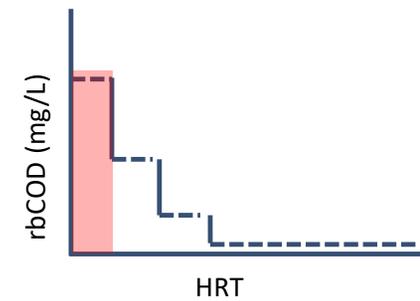
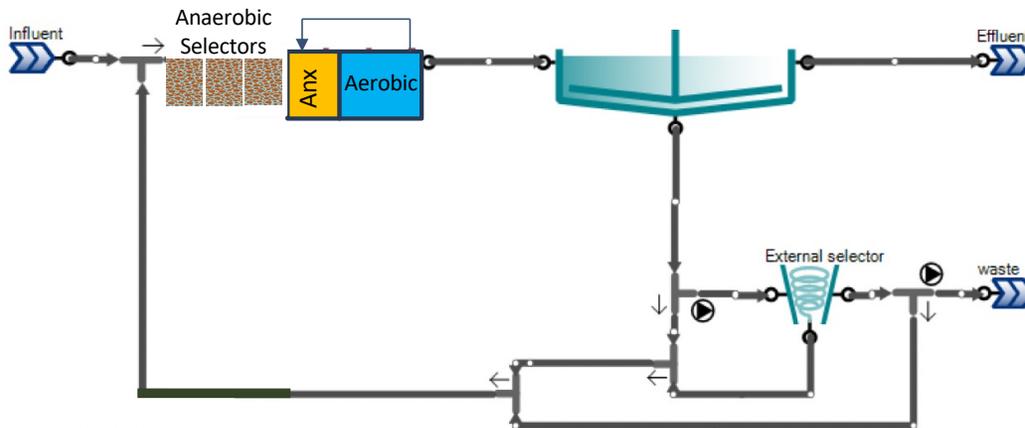


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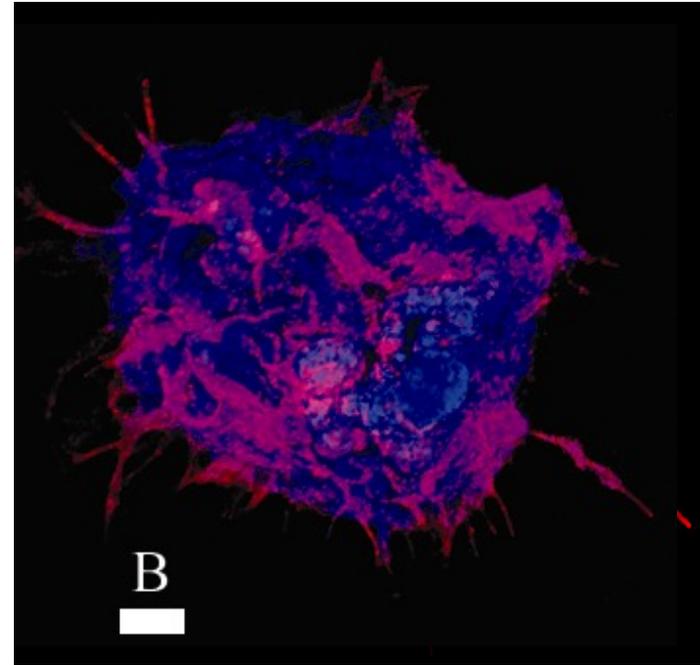
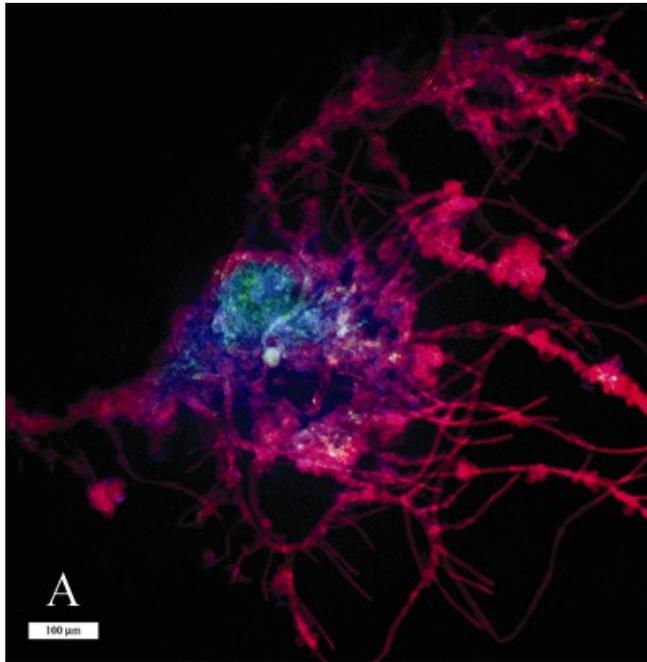
# Substrate Utilization in SBR vs Plug Flow



Continuous Flow configuration with high F/M selector



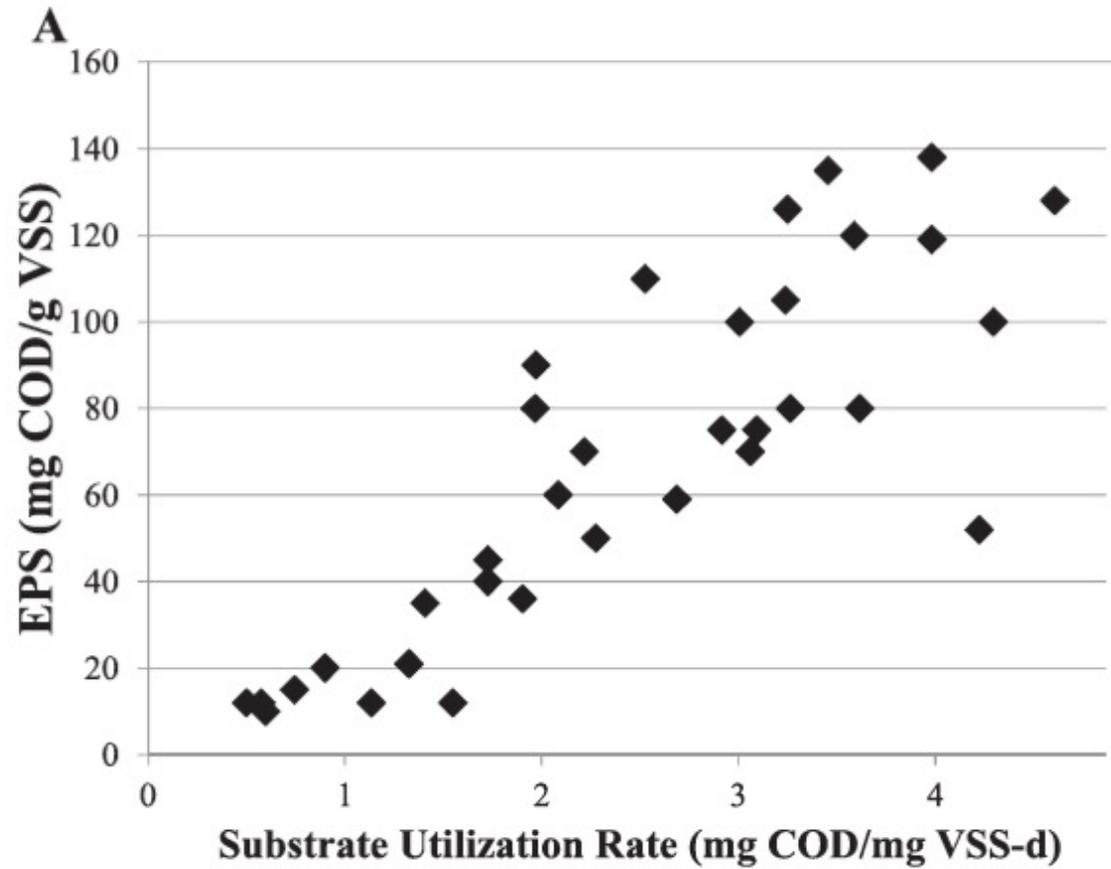
## Effect of F/M on EPS Formation



Scale = 100 μm

Cells  Polysaccharides - Bl  Proteins Gre 

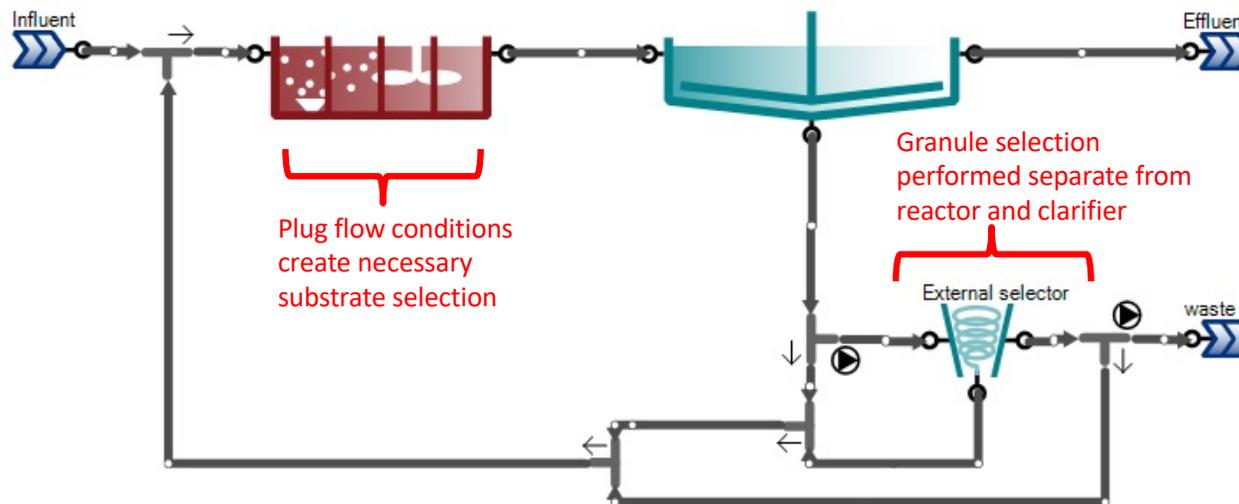
## Effect of substrate utilization on EPS and granulation



Jimenez (2015). *Water research*, 87, 476-482.

**Sludge densification may utilize a combination of biological and physical selection mechanisms**

# WRF Study Purpose: Granule Application in Continuous-Flow Systems



## Liquid-solids separation design must retain granules

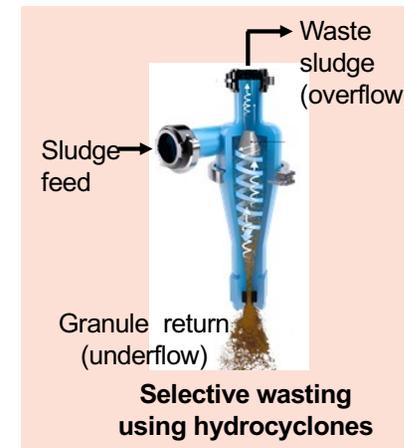
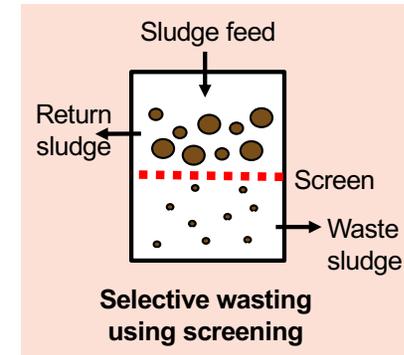
Favor **retention** of larger, faster-settling granules over flocs

Short settling times <10 minutes widely applied in SBRs

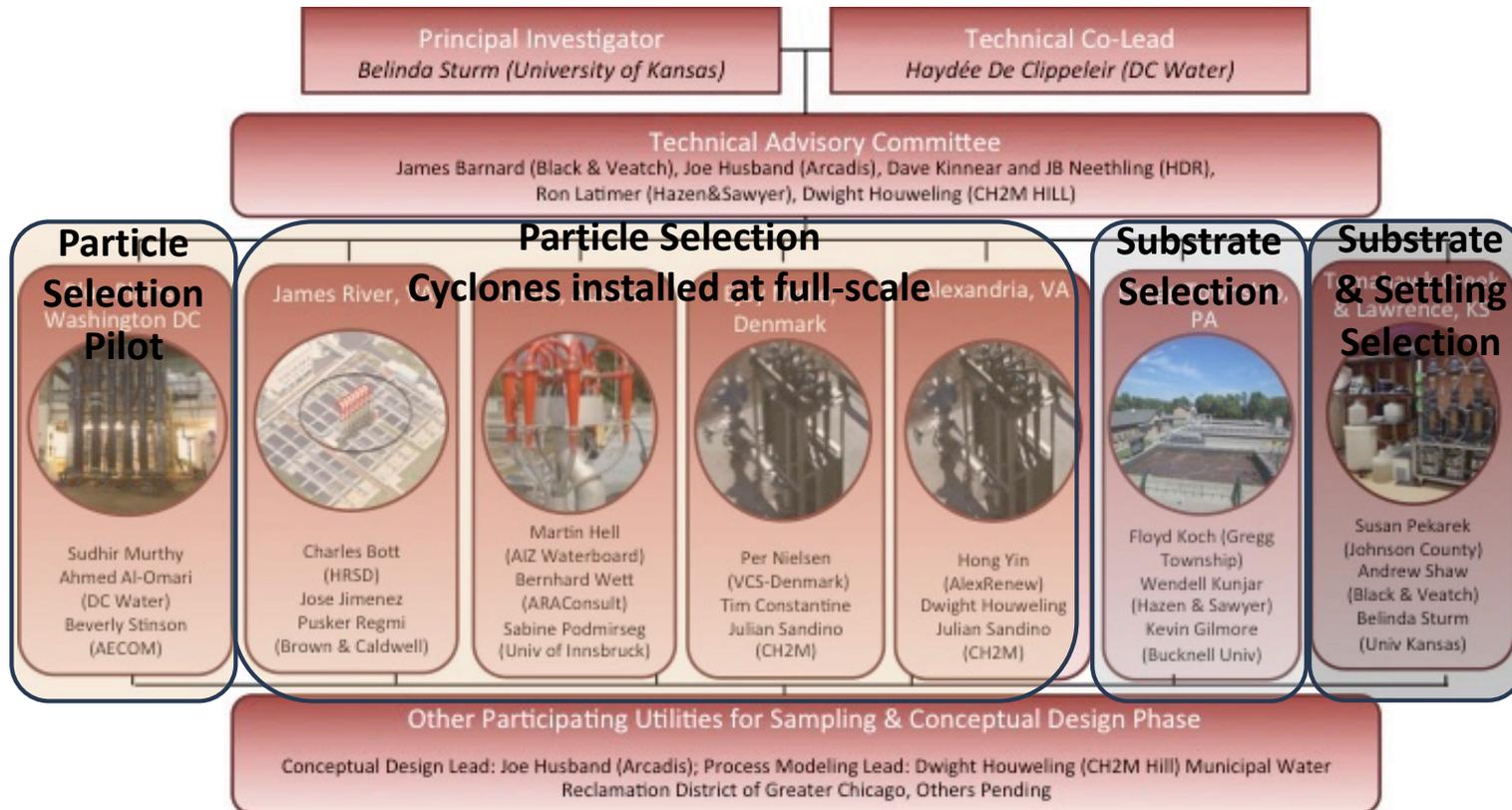
- “Selective settling pressure”
- “Hydraulic selection pressure”

Other approaches involving selective wasting

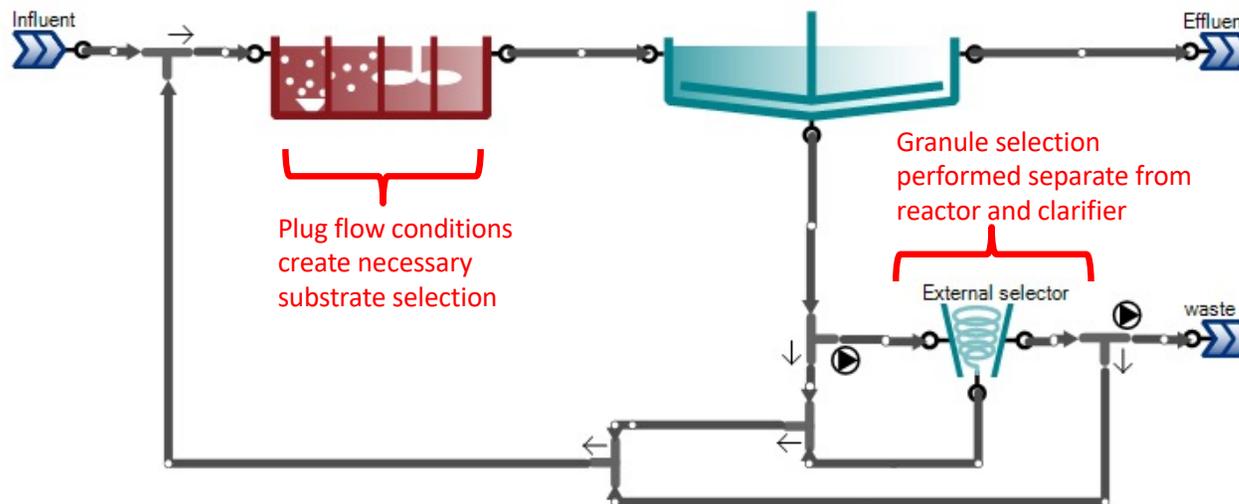
- Screens / Sieves (Liu et al., 2014)
- Hydrocyclones (Welling et al., 2015)
- Surface wasting (Barnard 2015)



# Water Research Foundation Project Overview



# WRF Study Purpose: Granule Application in Continuous-Flow Systems

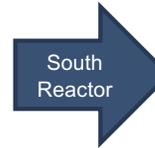


# Pilot Studies Manipulating F/M with Wasting

## Substrate Selection Only:

A target F/M is maintained by wasting mixed liquor daily (both granules and flocs wasted)

A mixture of granules and flocs are maintained in reactor

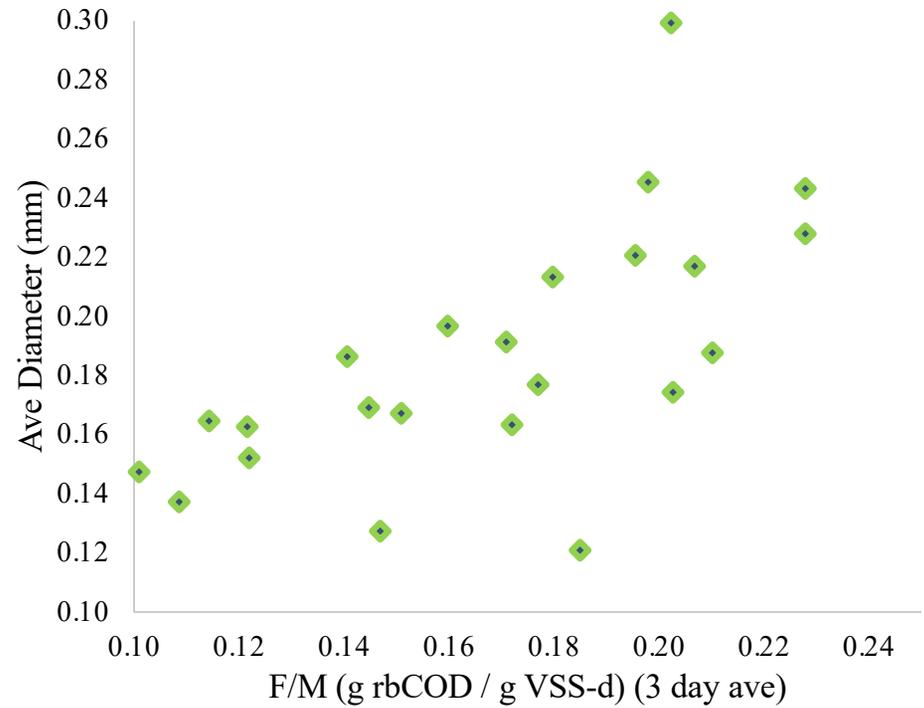
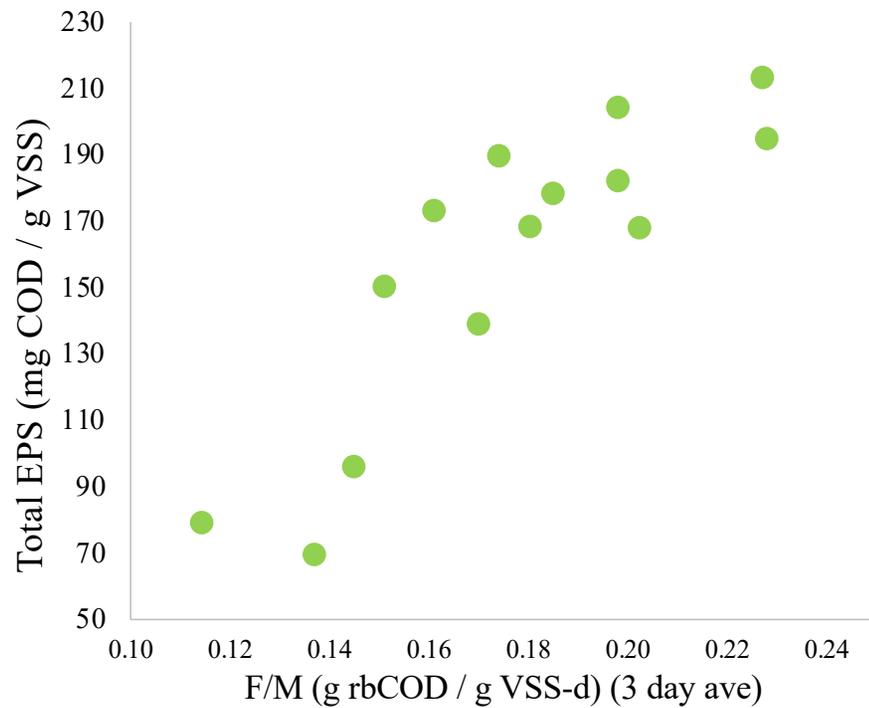


## Substrate & Particle Selection:

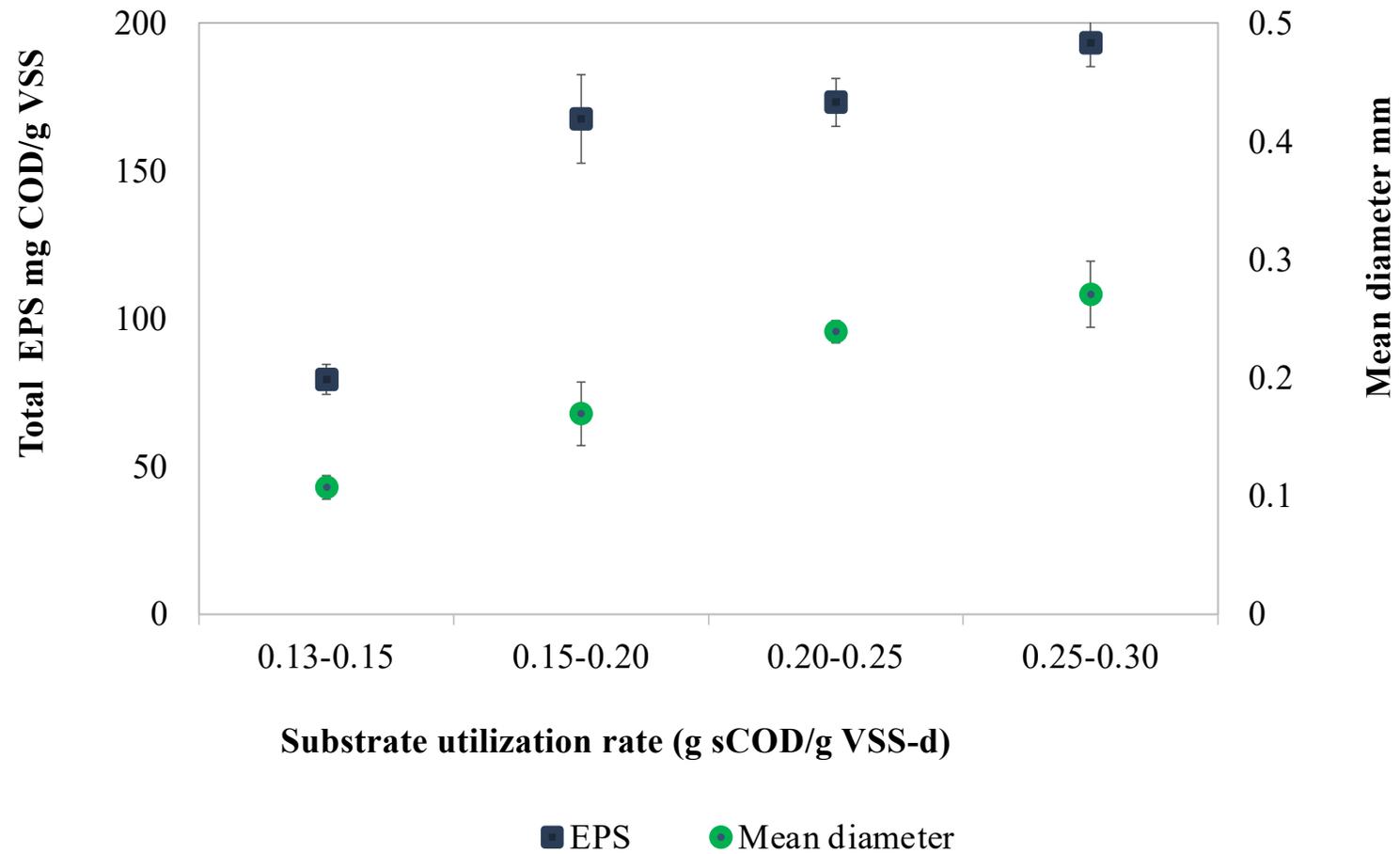
Daily biomass wasting is performed through a 0.2 mm sieve, and granules are retained

Mainly granules are maintained in the reactor

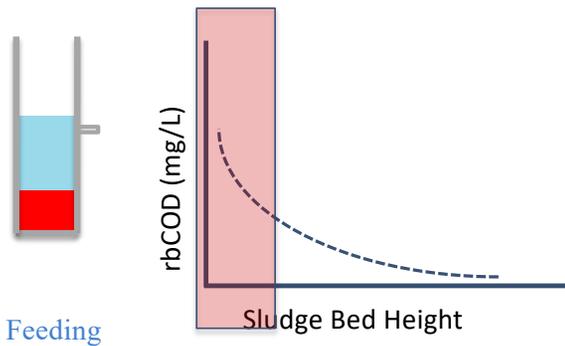
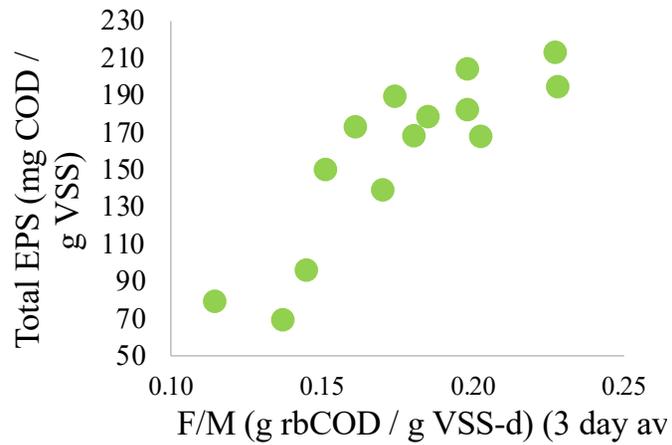
# Effect of F/M on EPS and Granule Formation



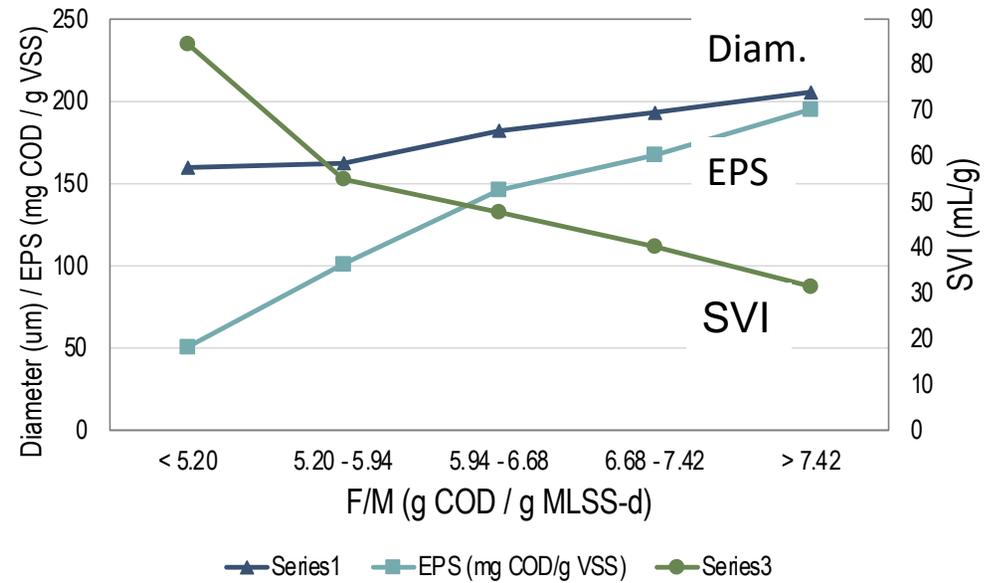
## Effect of substrate utilization on EPS and granulation



# Anaerobic or Metabolic Selectors



Anaerobic F/M –  
Assuming COD Uptake in First Selector Zone



# Experimental Plan

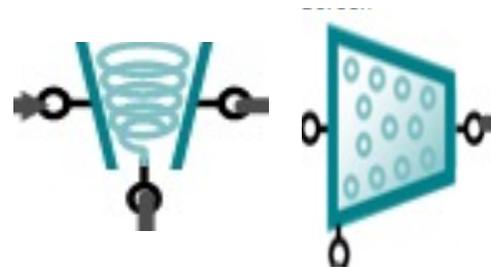


Aug. 15, 2015  
to Mar. 25, 2016

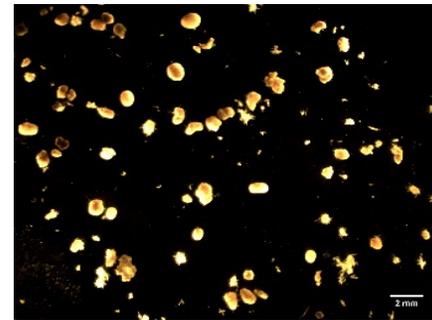
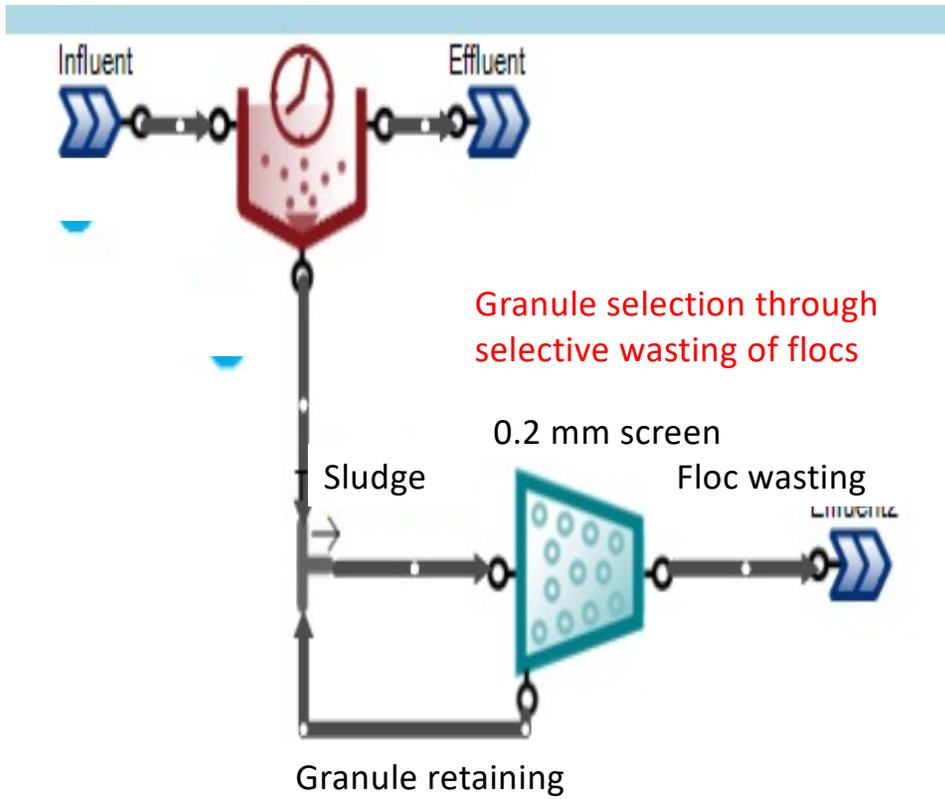
Mar. 25, 2016  
to Oct. 1, 2016

Granule formation  
and development

External selector  
implementation



# Selective Wasting



Retained fraction

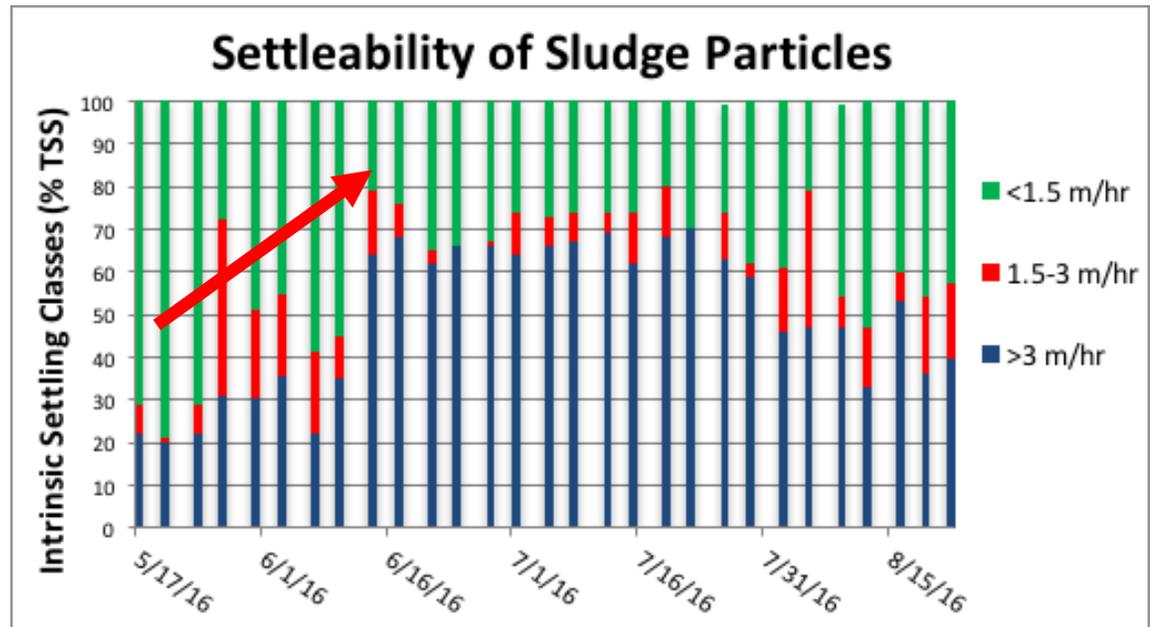


Wasted fraction

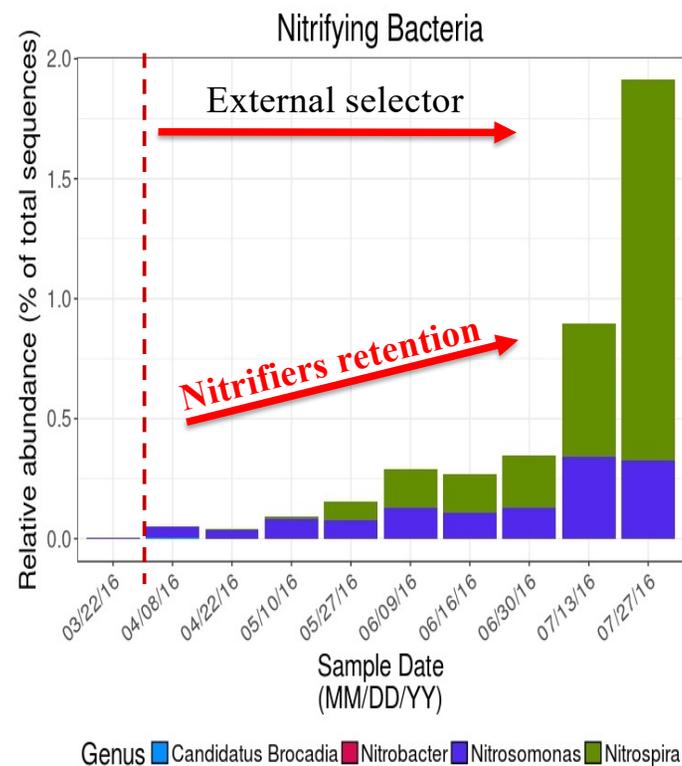
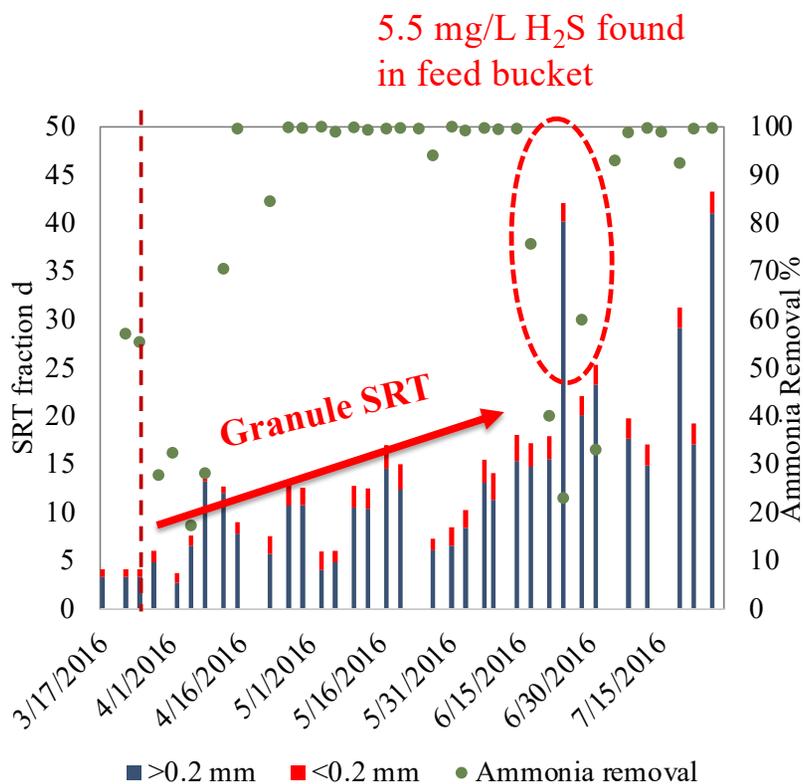
# Pilot Studies Manipulating F/M with Wasting

This graph shows the transition to mainly granule particles as the F/M > 0.21

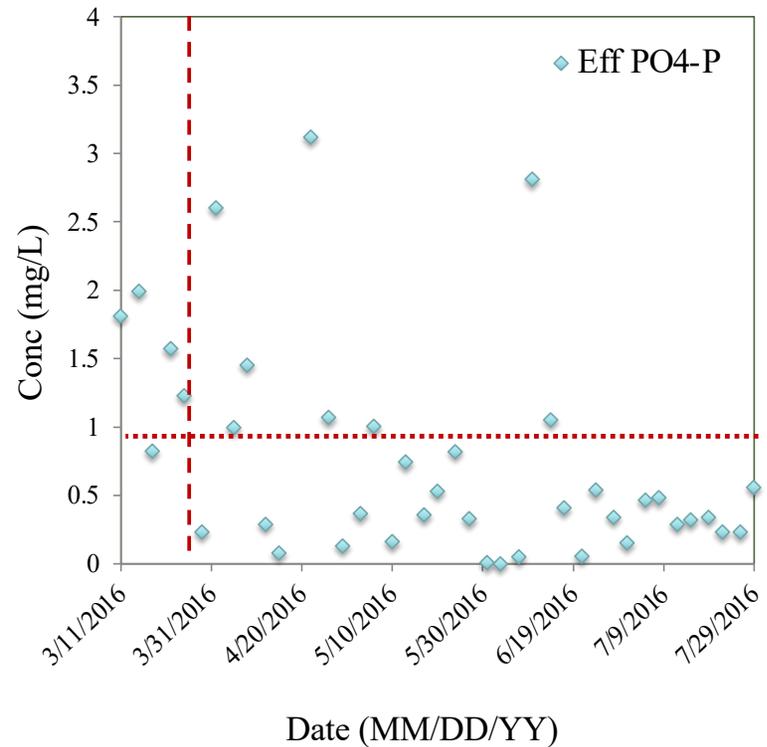
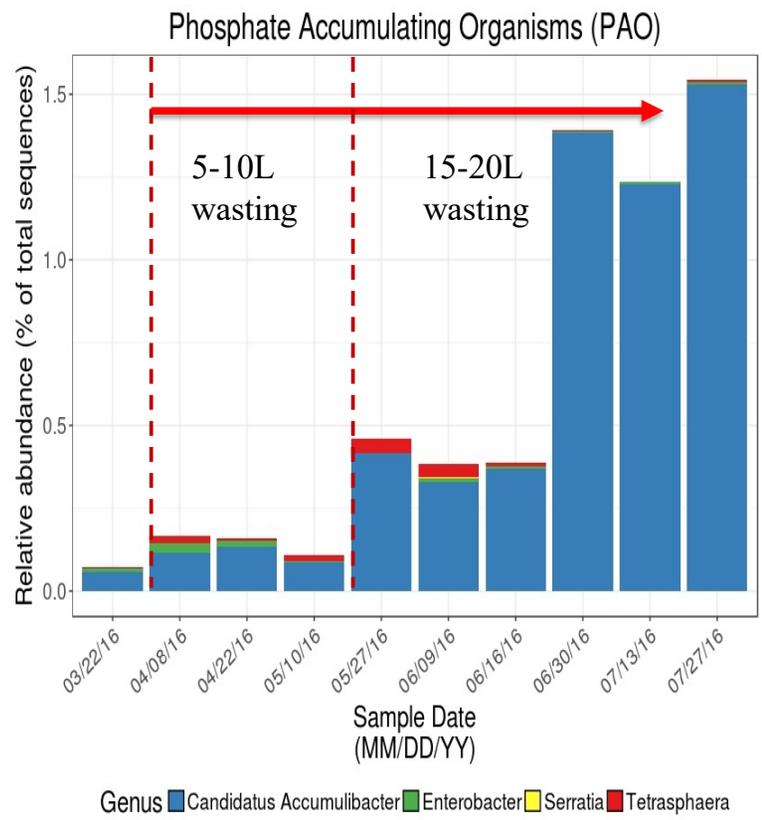
Increasing F/M  
Floc → Granule transition



# Impact of Selective Wasting on Sludge Structure

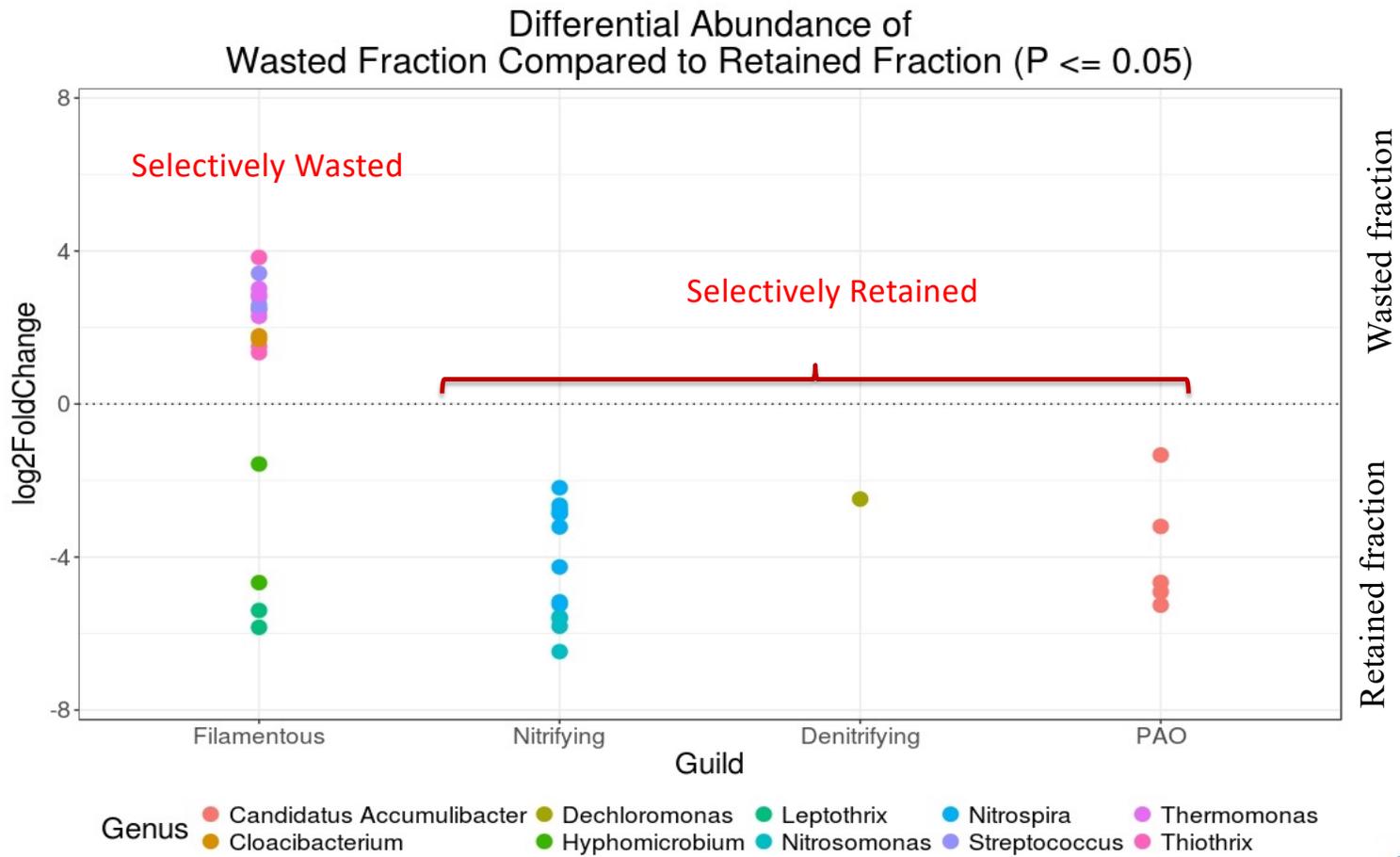


# Impact of Selective Wasting on Sludge Structure

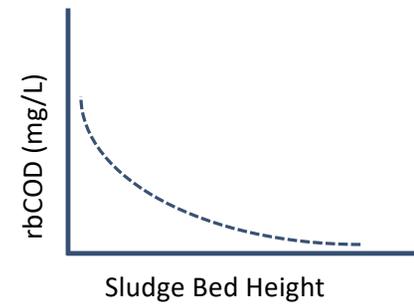
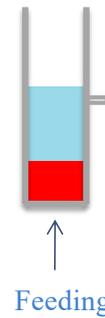


Granule retention → PAOs accumulation and phosphate removal improvement

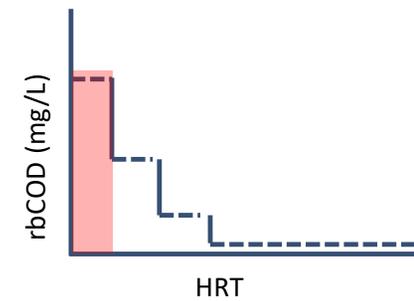
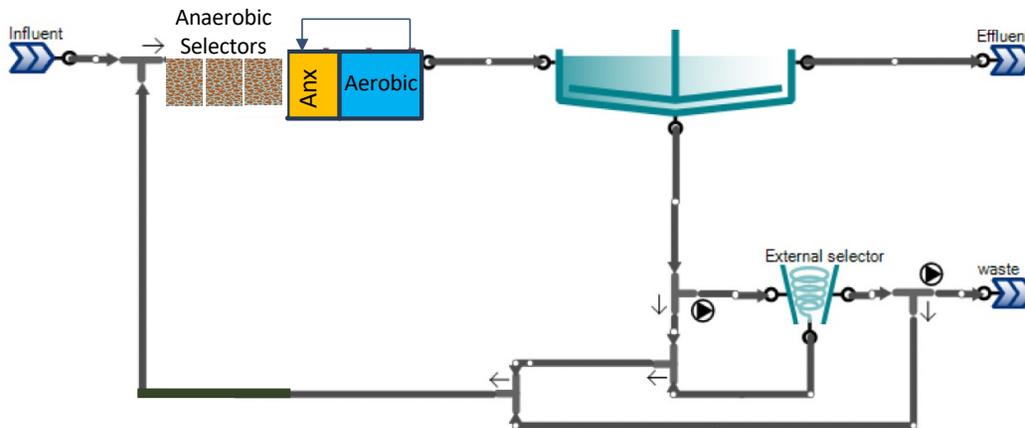
# Microbial Community Selection through Wasting



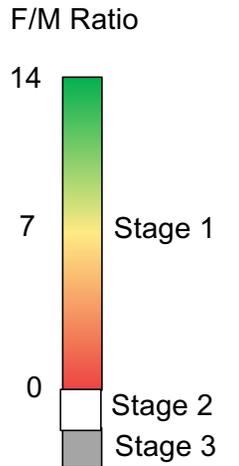
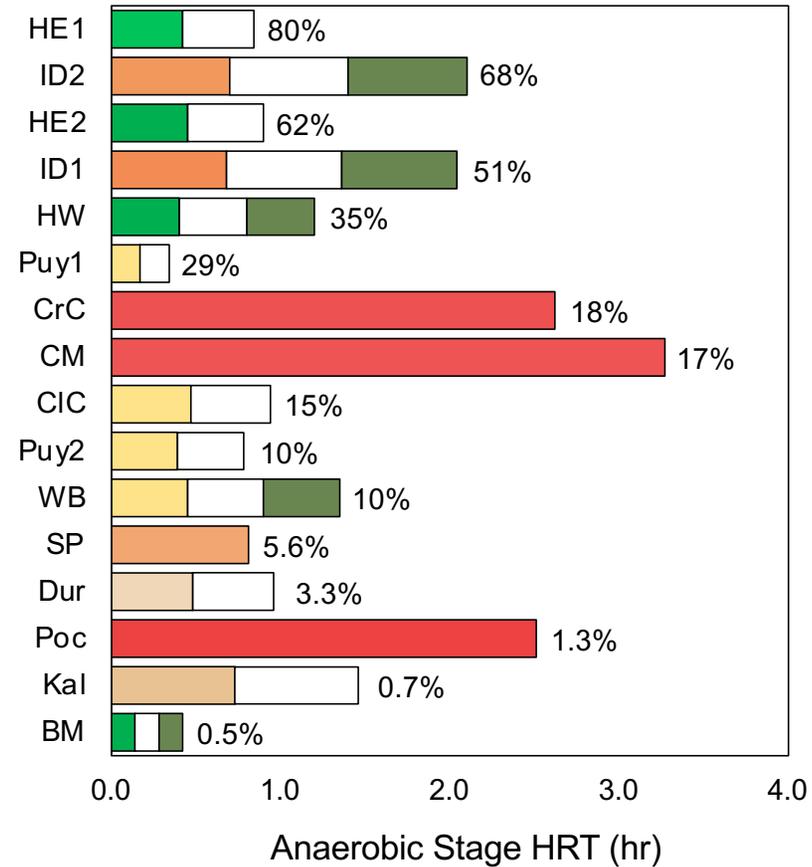
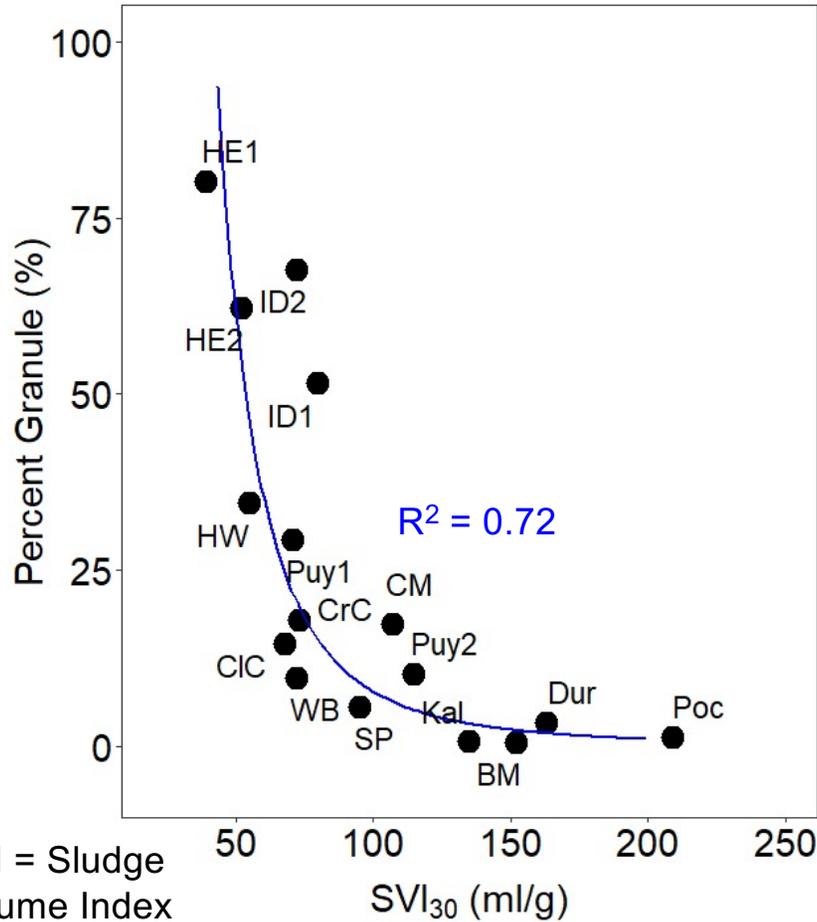
# Substrate Utilization in SBR vs Plug Flow



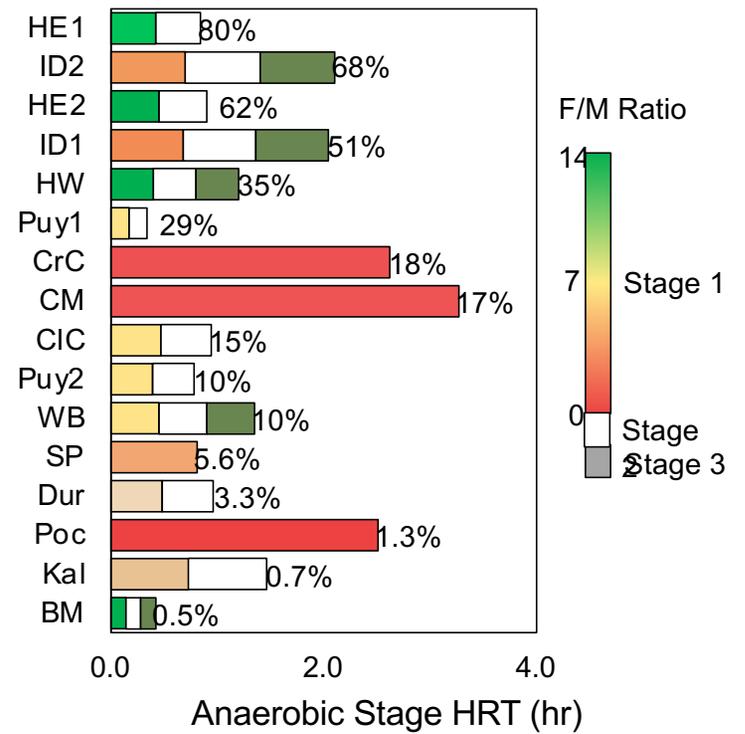
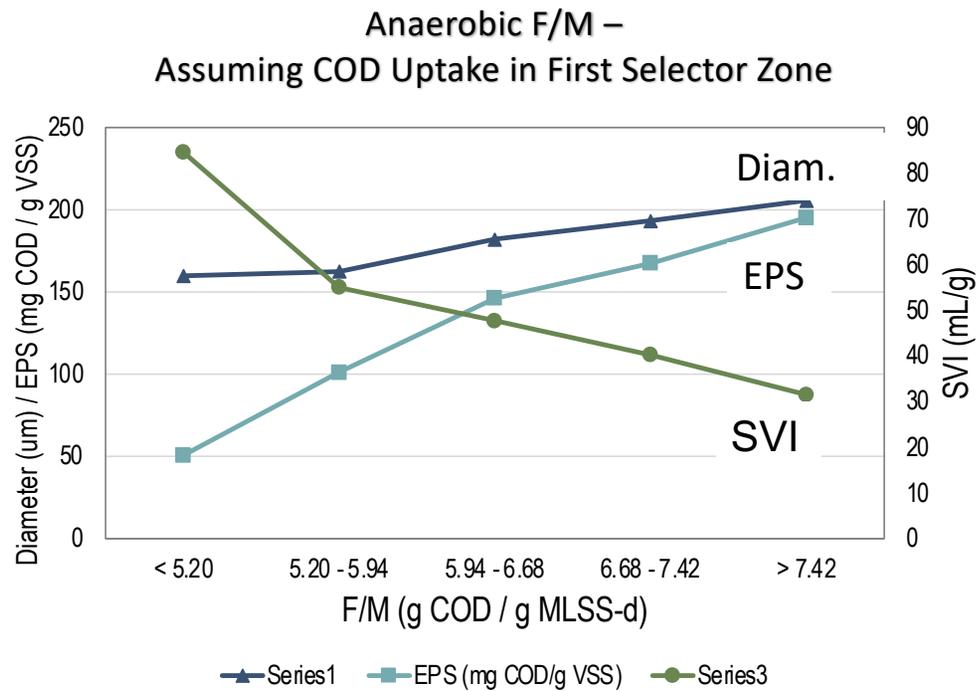
Continuous Flow configuration with high F/M selector



# Selection Factors Leading to Granule Growth at CFAS



# Anaerobic or Metabolic Selectors



Wei, S. P., Stensel, H. D., Nguyen Quoc, B., Stahl, D. A., Huang, X., Lee, P.-H., Winkler, M-K.H., 2020. Flocs in disguise? High granule abundance found in continuous-flow activated sludge treatment plants. Water Research

## Summary

Metabolic selectors should be designed to achieve high rbCOD uptake rates, with virtually complete rbCOD removal

An anaerobic F/M ratio greater than 5.2 gCOD/gVSS corresponded to higher EPS production; Anaerobic F/M greater than 7 has been associated with granulation

Microorganisms subjected to high F/M may accumulate substrate as internal storage products

It is possible to form granular sludge in continuous flow systems

## Future Work

As densification is achieved....

- How do existing clarifiers handle the additional solids loading rate?
- Full-scale experience with fines will provide confidence
- Implementation of hydrocyclones or screens to selectively waste flocs and retain granules has great potential
  - But operators need experience managing TWO sludge fractions separately



CBET-1512667



U1R14